

Secondary side corrosion of SG tube alloys in typical secondary side chemistries

OPEX of IGA/ODSCC (SG tube corrosion cracking)

- **600TT**

- More than 200 tubes affected worldwide
- Korea (1990+), USA (2002+), France (2012+)
 - Mostly at the top of tubesheet location

- **800NG**

- About 200 tubes affected in 2010 (IAEA)
- Sometimes after about 10 years of operation (4 years after TTS denting)

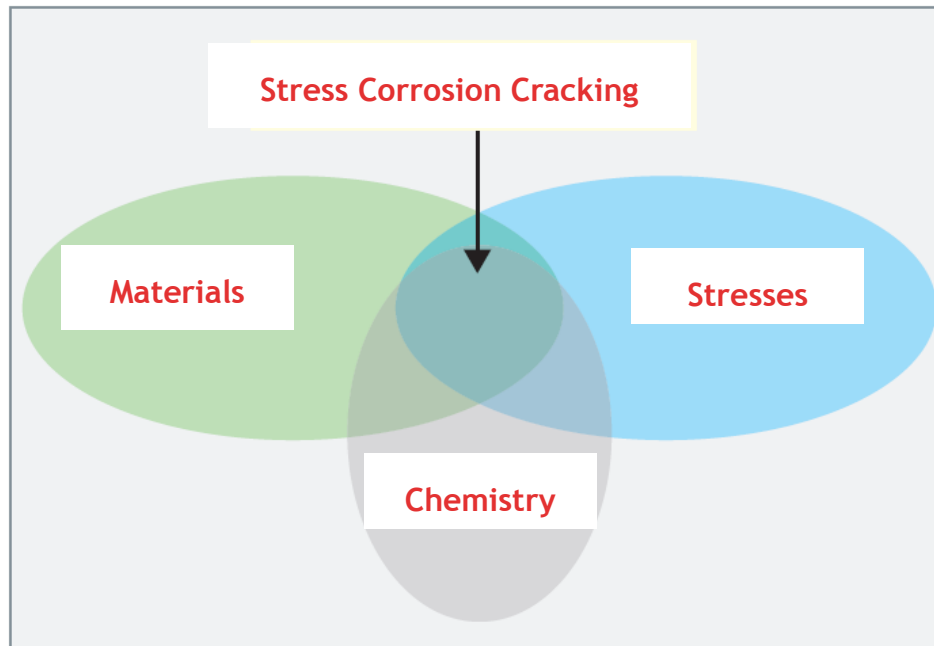
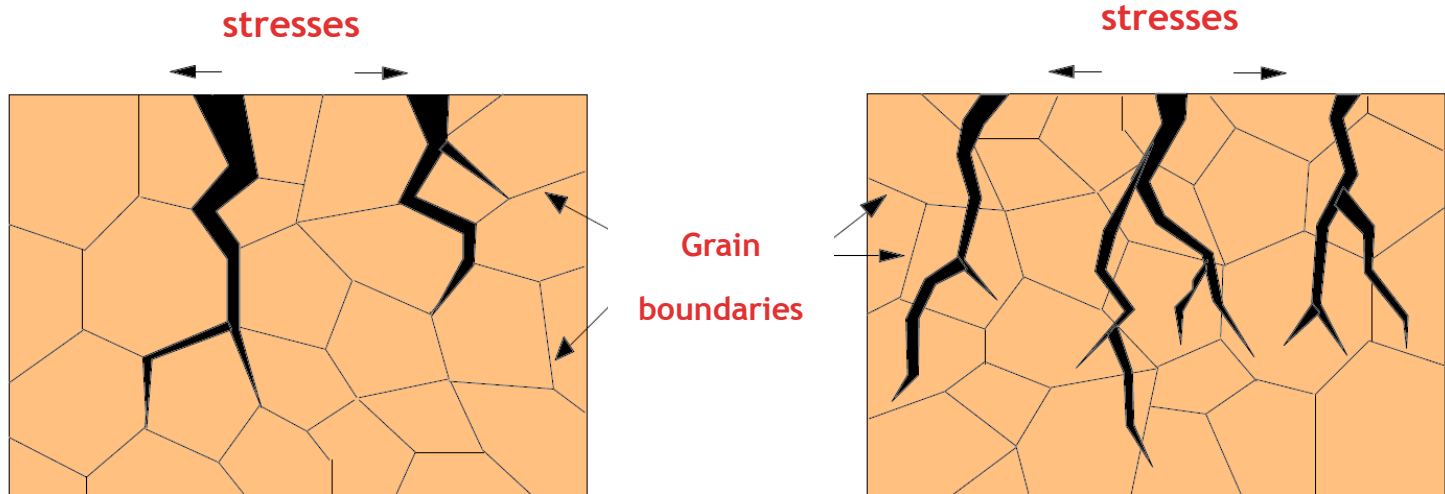
- **690TT**: nothing reported yet

- But dented tubes exist

- **Root cause analyses**

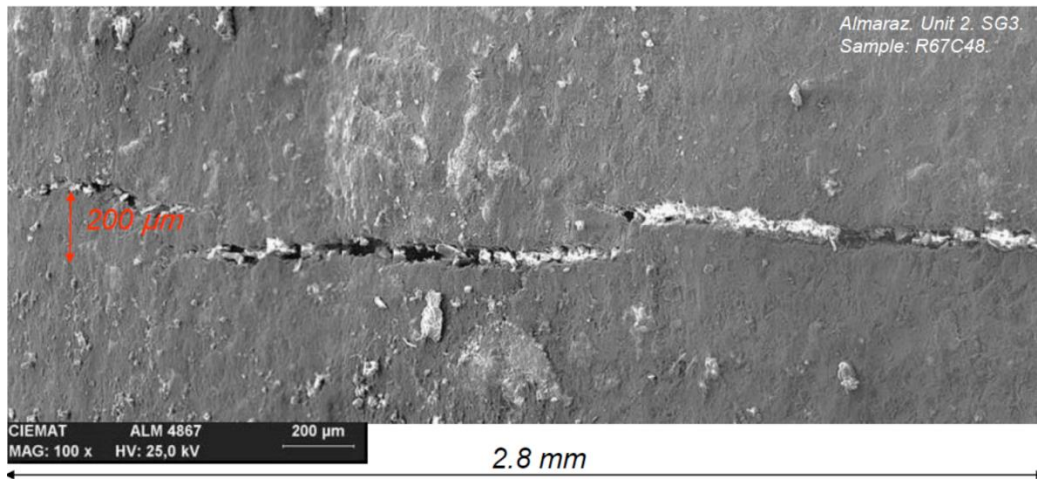
- Sometimes « non-optimized » microstructures
- Sometimes denting (TTS)
- Very often, Pb, S encountered. Also Al and Si

Insights on stress corrosion cracking



From CEA

Some recent ODSCC cracks

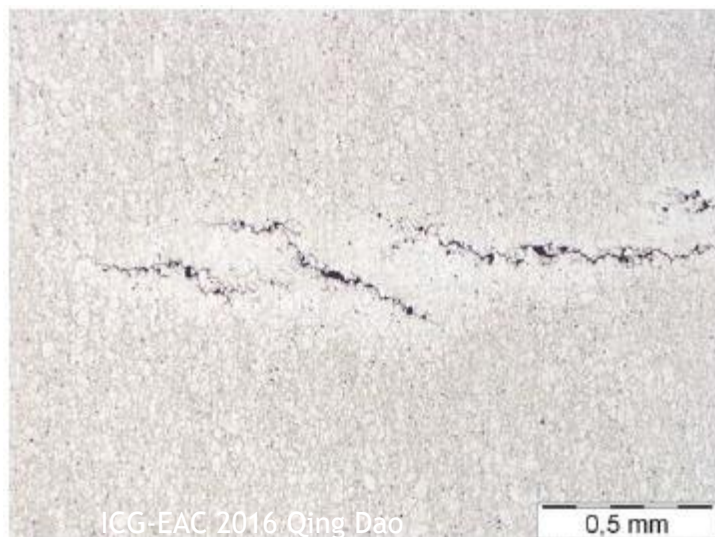


ODSCC in alloy 800NG tubes

Circumferential cracks network

12 years of operation

From Gonzalo, Fontevraud 8



ODSCC in alloy 600TT tubes

Circumferential cracks network

From Boccanfuso, 17th E. Deg

Safety stakes of IGA/ODSCC

➤ SGTR (steam generator tube rupture)

- Is one potential cause for core melting
 - Probability of 10^{-8} /reactor.year for a 1-2 tubes « small » SGTR
 - In addition high risk of radioactive product release to the atmosphere
- IGA/ODSCC
 - Affects thousands of tubes worldwide
 - Many instances of circumferential cracking
- Tougher detection by NDE than primary side cracks
 - Deposits, copper, TSP intersections...

➤ IGA/ODSCC, although limited on modern SG tubes alloys, remains a crucial safety issue

Stakes of IGA/ODSCC

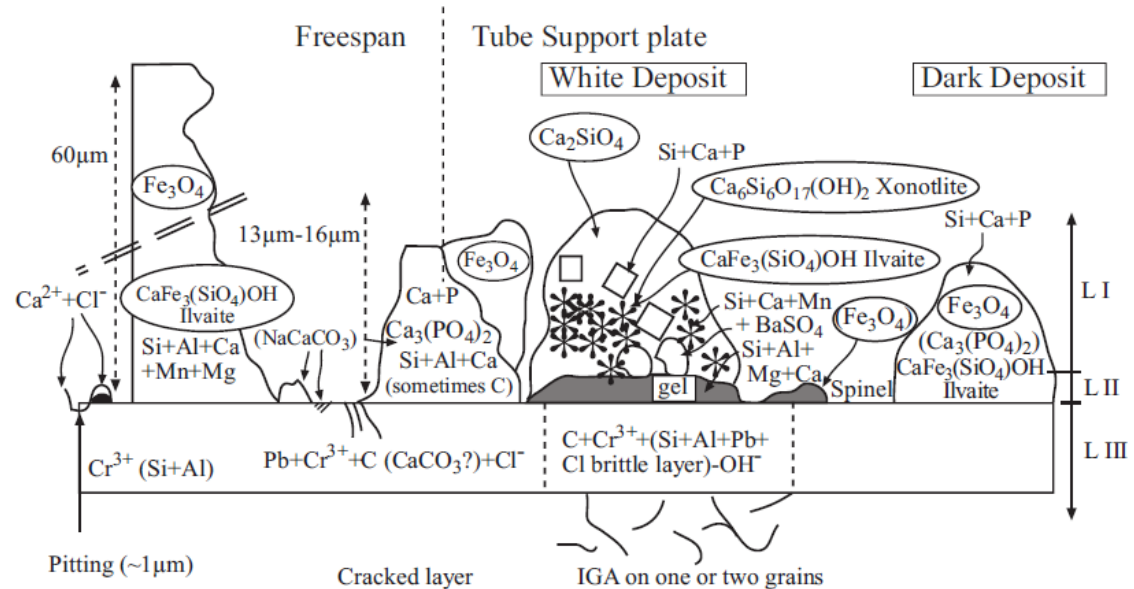
- R&D: risks of ODSCC exist
 - Even for corrosion resistant alloys
- OPEX for 600TT and 800NG
 - When ODSCC occurs, a few dozen tubes may be affected per SG
 - 2-3 affected tubes may be enough for a severe safety problem if SGTR
- Complexity of chemistries
 - No predictive modeling likely to be available
- Need for assessment tools
 - **Allowing plant chemists to specifically act**
 - Based on « **easy-to-access** » **data for utilities**
 - Actual chemistry: HOR (hide-out-return), sludge lancing analyses

➤ **Necessity of a domains of vulnerability approach**

Secondary side chemistry - insights

Secondary Water Chemistry

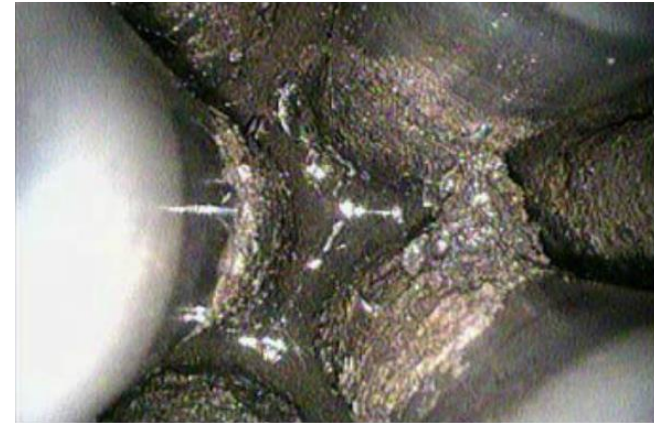
Role	Species	Conc., ppb
pH control	NH_3	X
O_2 decrease	N_2H_2	$\leq 8 \times \text{O}_2$
Leaks	O_2	< 10
Boil off remnant	H_2	1
Corrosion product	Cu	< 1
	Fe	< 5
Contaminant	Na	< 5
	Cl_2	< 10
	SO_4	< 10



- What is specified
- What is actually encountered on SG tubes
- Very complex local chemistries despite good operating procedures

What is a typical local secondary side chemistry?

- Analysis of OPEX over 25 years
 - Sludge lancing, HOR data...
- Many deposits/sludge at the TTS location, with a typical composition
 - Magnetite (Fe_3O_4) as balance
 - 2-10% **aluminosilicates**
 - <5 % of **calcium** species
 - 0.1 to 0.2%wt of **Pb** in sludge at the tube contact
 - Up to 1,4% of Pb in sludge collars (if pollution)
 - Presence of **S** (up to 10 000 ppm soluble from HOR)
 - Cu sometimes
- Crevice pH_T estimated by utilities
 - Multeq, OLI, MRI...
 - Ranging from **4 to 9** (range where test data are often missing)

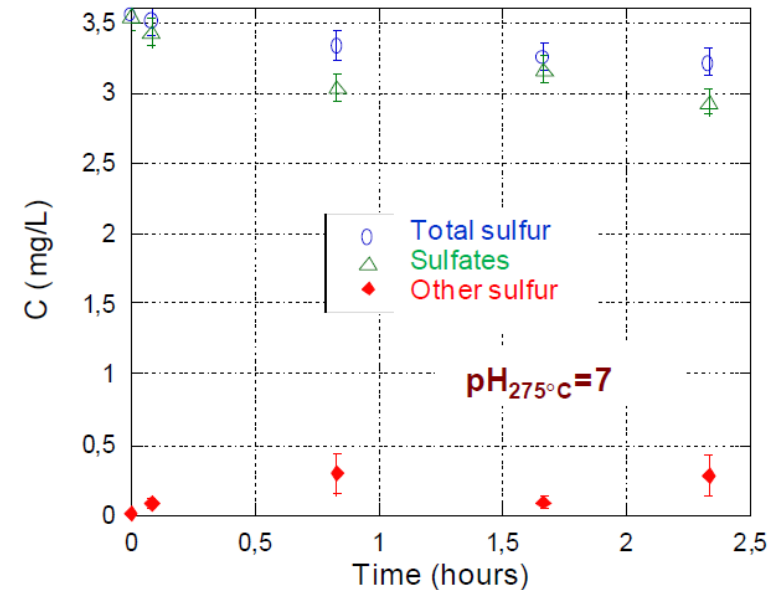


From Brechun, 2015

➤ No precise knowledge of what may happen in these conditions

The sulfur case

- Sulfates are measured at the SG blowdown
 - Sulfates in crevices may be 50 000x that measured during HOR
- In the operating SG, sulfates may be reduced
 - Magnetite, hydrazine...
 - Up to 10% of sulfur species in a « reduced » condition
 - According to pH_T



From Delaunay, 2012

➔ Need to consider some reduced sulfur species in tests

Test protocol

Materials

Industrial SG tubes
690TT, 600TT, 600MA

Specimens

RUB (1/6 SG tube)

- Pre oxidized in nominal AVT environment
- $\sigma \sim 550\text{MPa}$, $\varepsilon^p \sim 9\text{-}10\%$
9 specimens per capsule

Experimental setup

Capsule test

- Exposure 7000 h at 320°C
- Hydrogen removal
- Heat flux OD \rightarrow ID

Wet Steam

Resulting from the other conditions

Crevice simulating solution

- Nominal AVT environment
- Addition of NaCl essentially
- $4 < \text{pH}_T < 9$

Polluted sludge

Sludges « typical » from opex

- Al, Si, Ca
- Addition of Pb and/or S pollutions

Not too accelerated tests in representative secondary side chemistries

Material and test specimens

Chemical compositions

Material	Heat	C (%)	Si (%)	S (%)	P (%)	Mn (%)	Ni (%)	Cr (%)	Cu (%)	Co (%)	Ti (%)	Al (%)	Fe (%)
600TT	WF489	0.027	0.27	0.001	0.012	0.83	73.1	16.2	0.02	0.018	0.24	0.16	8.9
690TT	116201	0.017	0.173	<0.001	<0.015	0.33	58.0	29.84	<0.01	<0.035	0.37	0.048	11

Fullfill the RCC-M requirements

Test specimens : Reversed U Bend

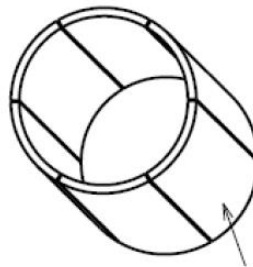
RUB (1/6 SG tube)

Pre oxidized in nominal AVT environment

$\sigma \sim 550 \text{ MPa}$, $\varepsilon^p \sim 9-10\%$

9 specimens per capsule

6 sections per tube



Test matrix

I Type of environment

Sludges : Fe_3O_4 + 0,8% CaO + 5% of $\text{Al}_2\text{O}_3/\text{SiO}_2$ with Si/Al=4

Liquid phase: H_2O + 3ppm ETA + 1 ppm NH_3 + 3M NaCl + N_2H_4

- pH_T and type of pollution

	$\text{pH}_T = 4$	$\text{pH}_T = 7.5$	$\text{pH}_T = 9$
2000 ppm of Pb in sludge as PbO	✓	✓	✓
2000 ppm of Pb in sludge as (91% PbSO₄ 9% PbS)	✓	✓	✓
8000 ppm of soluble SO_4^{2-} as (91% Na₂SO₄ and 9% Na₂S)	✓	✓	✓
Pb/S free sludge	✓	✓	✓

pH_T adjusted by NaOH or HCl/ H_2SO_4 based on thermodynamical simulations

Global preliminary results

		pH _T = 4			pH _T = 7,5		
		WF422 600MA	WF489 600TT	116201 690TT	WF422 600MA	WF489 600TT	116201 690TT
Pb (PbO)	Solid	c	c		c		
	Liquid	-		C	-	-	-
	Steam	-		C	-	-	-
Pb and S (PbSO₄/PbS)	Solid	C	C		C	C	
	Liquid	-	C	C	-	C	
	Steam	-	C	C	-	C	
S (Na₂SO₄/Na₂S)	Solid	C					
	Liquid	-	C	C	-		
	Steam	-	C		C	C	-

No analysis

-

GC and/or IGA

No indications

C



Cracks
observed from
the surface

**Test at pH_T 9 not yet finished
December 2016**

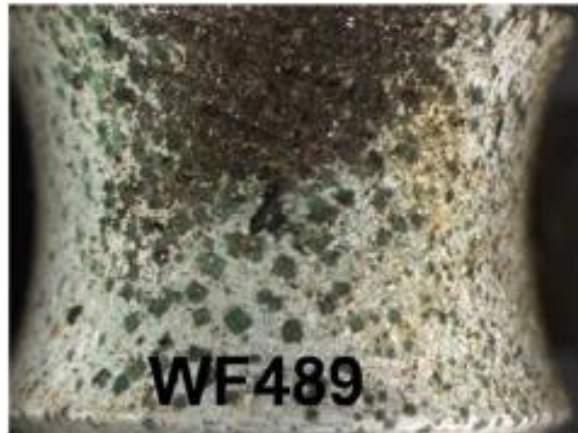
➤ Examination of specimen

Optical examination – $\text{pH}_T = 4$ – liquid phase

No observable sign apart from oxidation



PbO



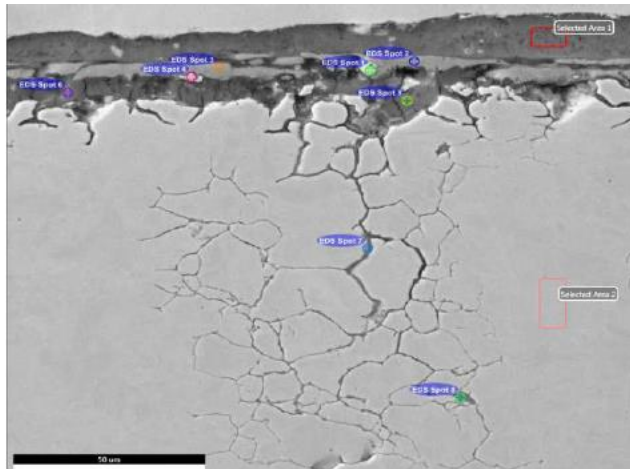
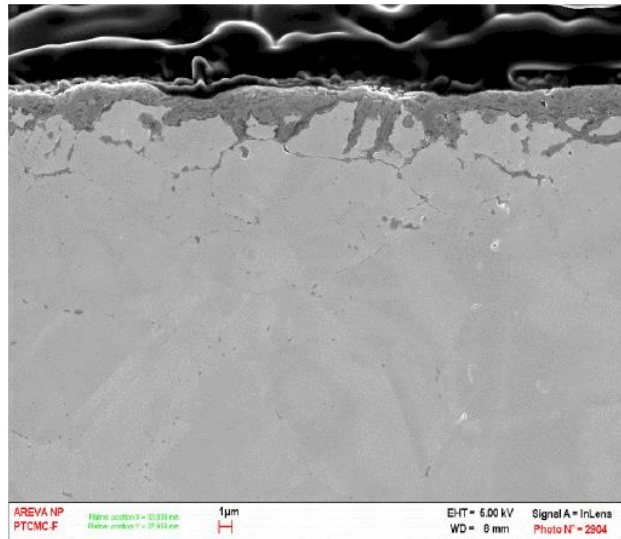
PbSO_4

600TT

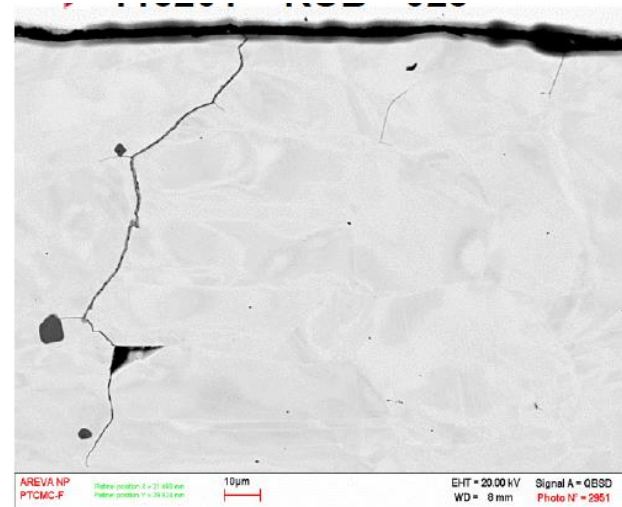
690TT

SEM cross sections – $\text{pH}_T = 4$ – liquid phase

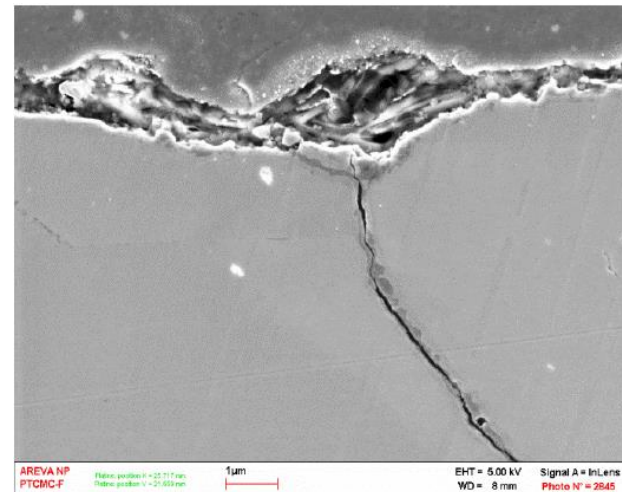
IGA, IGSCC and GC (600TT) vs IGSCC (690TT) confirmed



600TT



PbO



PbSO₄

690TT

SEM cross sections – pH_T = 4

Summary

		600TT		690TT	
		Max. depth	Crack density* (/ mm)	Max. depth	Crack density* (/ mm)
PbO	Liquid	180 µm	2	110 µm	0.9
	Wet steam	20 µm (IGA)	/	63 µm	0.5
PbSO₄	Liquid	180 µm	~3	60 µm	0.7
	Wet steam	78 µm	1	45 µm	0.32
Na₂SO₄	Liquid	79 µm	0.7	92 µm	0.2
	Wet steam	31 µm	0.3	/	/

* Depth > 15 µm, specimen width ~10 mm

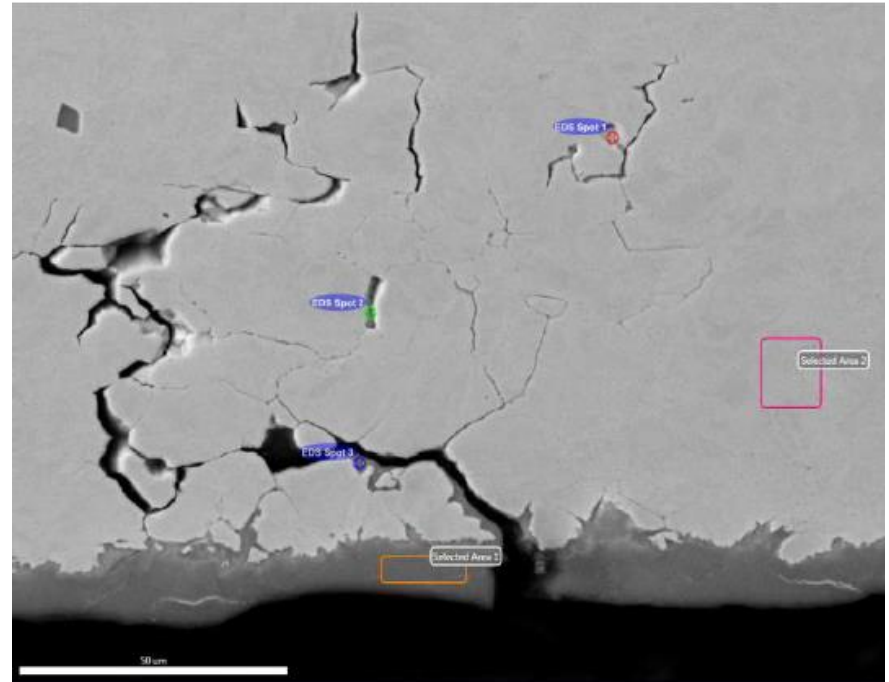
SEM chemical analyses – $\text{pH}_T = 4$

IGA, IGSCC and GC (600TT) vs IGSCC (690TT) confirmed

SEM - EDS

- No Pb or S apart from traces
- Al, Si clearly detected

600TT
 PbSO_4
sludge

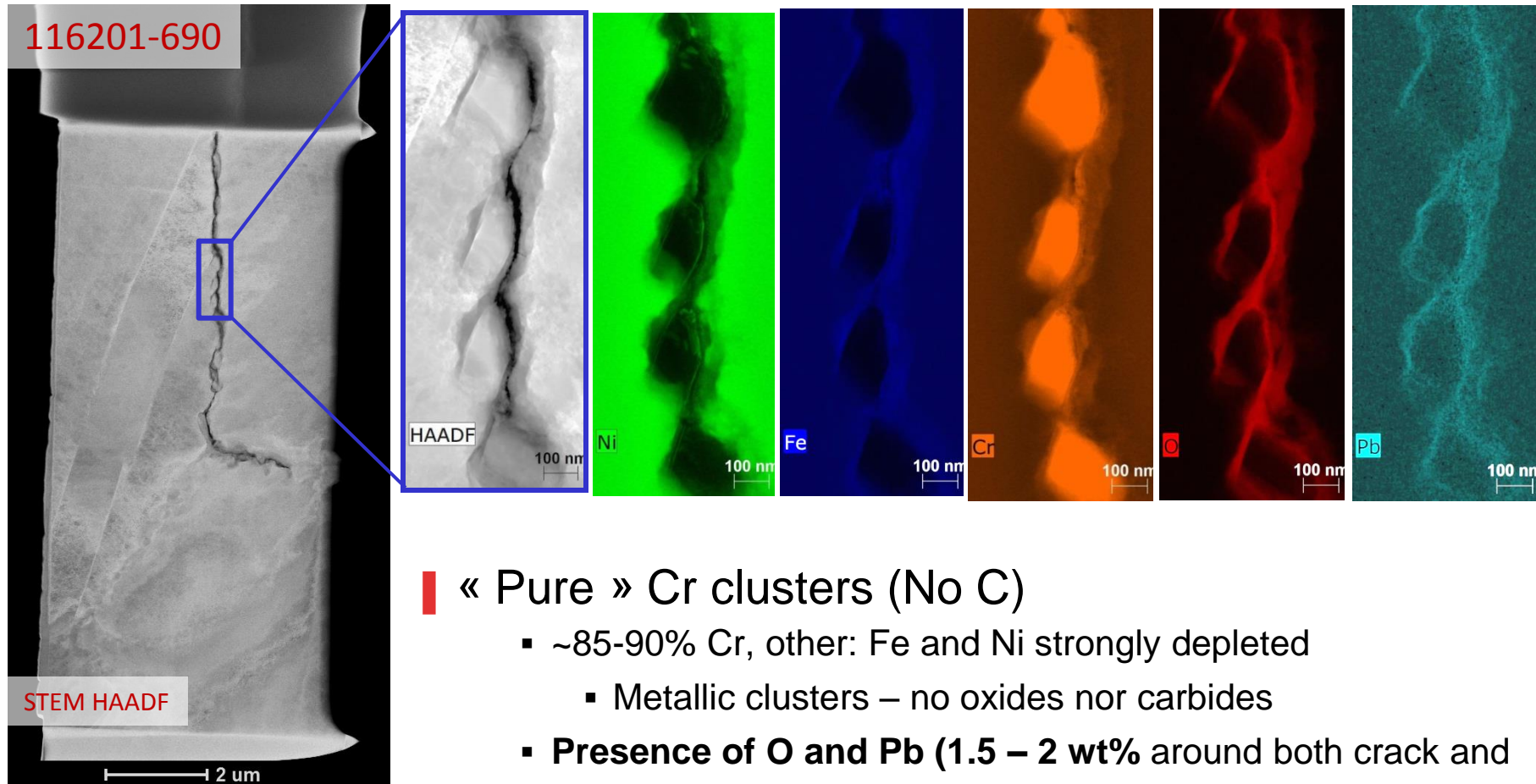


	O	Mg	Al	Si	S	Ca	Ti	Cr	Fe	Ni	Pb
WF489-027 Area 1 EDS Spot 1				0,7				16,8	9,6	72,9	
WF489-027 Area 1 EDS Spot 2	2,7	1,7	1,1					17,6	9	67,9	
WF489-027 Area 1 EDS Spot 3	1,6		1,4	0,6				16,6	9,3	70,5	
WF489-027 Area 1 Selected Area 1	21,8		0,6	1,3		0,5	0,5	27,1	15,8	31,5	0,7
WF489-027 Area 1 Selected Area 2	1,5			0,7				16,8	9,3	71,7	

➡ **TEM**

TEM – 690TT – PbO – pH_T 4 – liquid phase

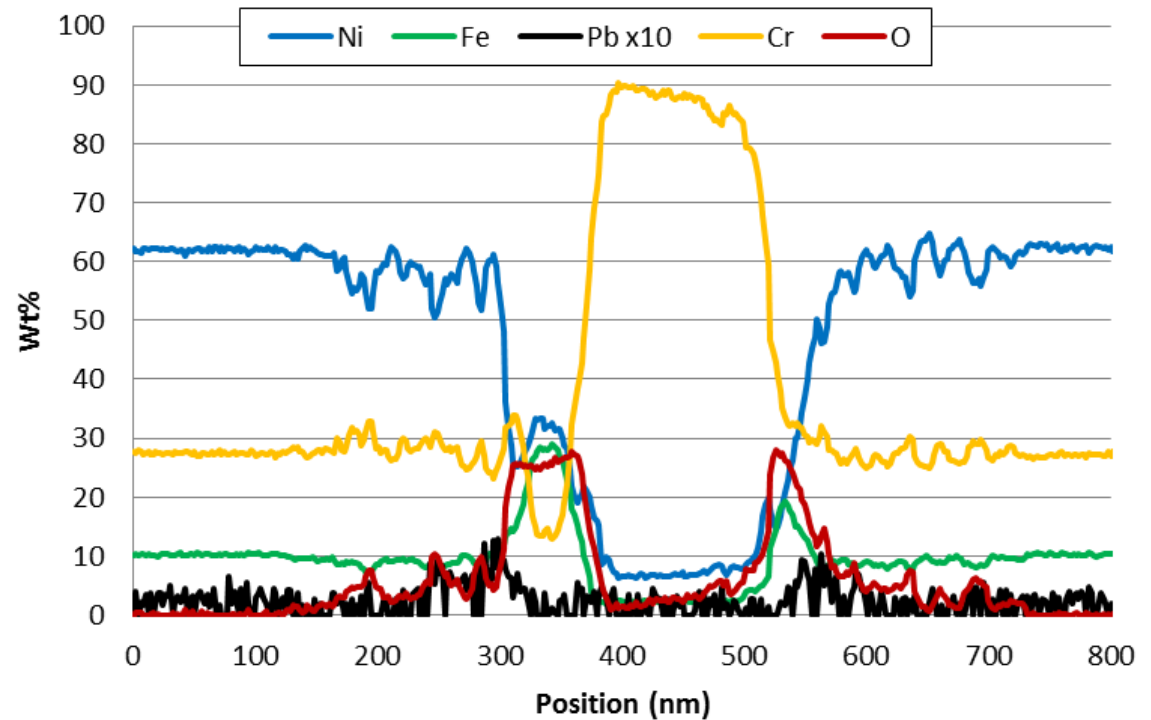
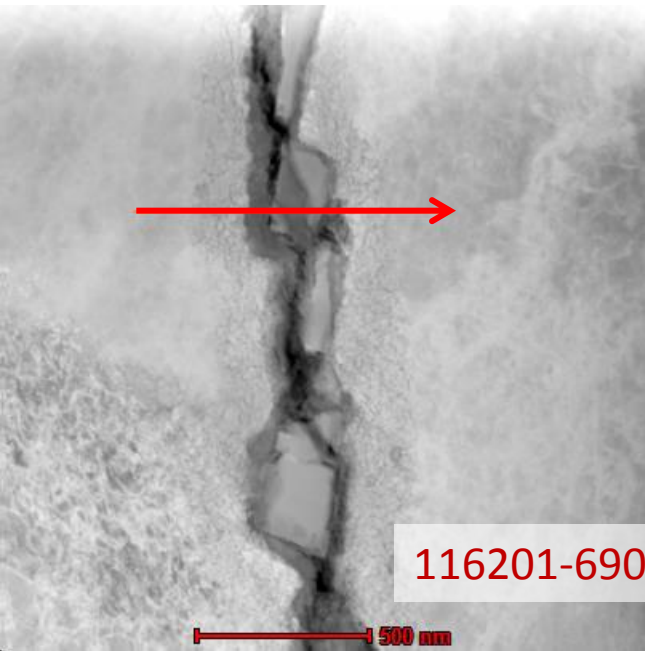
EDX – ChemiSTEM of the crack



« Pure » Cr clusters (No C)

- ~85-90% Cr, other: Fe and Ni strongly depleted
 - Metallic clusters – no oxides nor carbides
- **Presence of O and Pb (1.5 – 2 wt% around both crack and Cr rich clusters)**

TEM – 690TT – PbSO₄ – pH_T 4 – liquid phase



- « Pure » Cr clusters
 - Surrounded by oxides
 - Alloy disturbances prior to oxidation
- Pb at the metal/oxide interface
 - ~1% wt of Pb

Conclusions (1/2)

➤ IRSN performed corrosion tests on SG tube alloys

- In typical local secondary side environments
 - Based on opex from 20 years of sludge analysis
 - pH_T in the range quoted by utilities, 4, 7 and 9
- Two goals
 - Identifying domains of vulnerabilities in « typical » chemistries
 - Understanding potential damage mechanisms
- pH_T 4
 - All alloys suffer from corrosion
 - **GC, IGA and IGSCC** (IGSCC only for 690TT)
 - Alloy 690TT is not immune and IGSCC (no TG) could be encountered, even with S alone (no Pb)
- pH_T 7.5 and 9
 - Pending results - Already 600MA and 600TT susceptible at pH_T 7.5

Conclusions (2/2)

- Examinations confirm the involvement of Pb and S in the currently observed damage
 - 2 potential mechanisms currently assumed
 - Research work going on
- Tests performed identify potential risks
 - Confirmed by OPEX (600TT)
 - Increase the available knowledge for assessing the risk of currently operating components